

Automating suspended solids control helps a plant maintain consistent nutrient removal

Robin E. Bain and Walter S. Johnson

Clark County Sanitation District treatment plant in Las
Vegas, Nev., was recently expanded to meet growth demands and new ammonia permit limits—a wasteload allocation approximately equivalent to 0.71 mg/L. The plant includes an activated sludge process consisting of eight 11-mgd (41 635-m³/d) acration basins, each with a dedicated secondary clarifier.

During the plant's first year of operation, staff achieved biological phosphorus removal in aeration basins by shutting off the mixed-liquor recycle into the anoxic zones, which provided for denitrification primarily to restore alkalinity.

The cost savings from reduced chemical usage and solids production were substantial (\$52/ton, or \$57/Mg) and sustainable as long as biological phosphorus removal was consistent. Encouraged by the cost savings, staff investigated process control techniques to maintain reliable biological phosphorus removal.

### Conventional Control

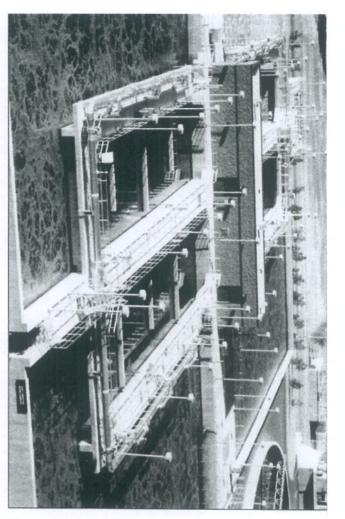
In any activated sludge process, maintaining mixed liquor through diurnal flow patterns is a key performance parameter. Waste activated sludge (WAS) flow rates determine the mixed liquor suspended solids (MLSS) concentration. At Clark County, operators initially followed the conven-

After being moved to several locations, a probe that measures mixed liquor suspended solids was placed in the oxic zone in the corner of the lagoon — far from excessive air turbulence, but close enough to maintain minimum velocities across the probe.

tional procedure of controlling solids inventory by collecting a grab sample of mixed liquors and then analyzing the MLSS concentration. After establishing a target MLSS, operators used a simple algorithm to calculate the new wasting rate (Q<sub>WAS</sub>), as follows:

New  $Q_{WAS} = Previous Q_{WAS} \times [actual MLSS]$  (grab sample) + target  $MLSS]^{0.5}$ 

(The square root smooths out the multiplication factor and reduces the shock of change on the biological system.) After determining the new wasting rate, staff would manually adjust



the valve position. However, phosphorus and ammonia removals were inconsistent, so they took a closer look at the activated sludge process.

# **Problems With Grab Sampling**

solids concentrations. a substantial range of actual suspended RASSS for a 2-week period, and found hourly sampling of the MLSS and ent removal problem, staff conducted data. To identify the cause of the nutrichosen primarily to make up for the lar day. The 7-day averages had been determine wasting rates for a particua.m. and calculate a 7-day average to ple from each basin between 6 and 9 sludge suspended solids (RASSS) sam-MLSS sample and a return activated Normally, operators would grab an of better, more representative

could vary by ±15%, and the RASSS taken anytime between 6 to could not be performed more than tor time and, procedure required substantial operathe inconsistencies. In addition, the grab samples was potentially a cause of that adjusting wasting rates based on sample by ±40%. Operators realized diurnal samples, an MILSS grab sample age MLSS in the basins, as seen in the an art. Compared with the actual averthrough WAS flows has always been dure, manually adjusting mixed liquor As a time-delayed, reactive for practical reasons. 9 a.m. proce-

twice a day. Staff began seeking a way to obtain real-time MLSS data, with the ultimate goal of being able to automatically control mixed liquor through the on-line instrumentation and a distributive control system (DCS) system.

#### **Integrating Probes**

quency of cleaning. using the on-line device, months, staff monitored actual MLSS cation reduced probe fouling and fremaintained across the probe. This loties of 2 ft/sec (0.6 m/sec) could be the oxic zone, 4 ft (1.2 close enough so that minimum velocifrom excessive air turbulence, but surface and far enough horizontally eral locations, the device was placed in computer. After being moved to sevslurry and send data to the plant's signed to analyze suspended solids in meter, and transmitter that was debasin a device consisting of a probe, Operators installed in an aeration For severa m) from the compared

<b>Cost of the Automatic Control System</b>	stem	
Description	With	Without
Annualized Capital Costs <sup>1</sup>	\$13 560	\$0
Annual Operation and Maintenance Costs		
<ul> <li>monitoring and controlling WAS</li> </ul>		
flow and activated sludge process	\$2 4502	\$42 0503
lab supplies	\$2604	\$3 620
electricity	\$2705	\$0
TOTAL	\$16 540	\$45 670
Annual cost savings:	\$29 130/yr	)/yr
Payback: $$91\ 000^6 \div $29\ 130 = 3.1\ years$		

- The capital recovery factor is 0.149, based on a 10-year lifetime and 8% interest.
- Operator time to calibrate and clean probes is 3 hr/d every 14 days, or 0.21 hr/d. Personnel costs (including salary, benefits, uniforms) are \$32/hr. 0.21 x 32 x 365 days = \$2450/yr.
- <sup>3</sup> Operator time to collect samples, perform lab tests, and calculate adjustments was 3.6 hr/d.  $3.6 \times 32 \times 365 = \$42 \ 050 \text{/yr}$ .
- <sup>4</sup> Lab supply use was reduced also because tests would be run once every 14 days for calibration instead of every day.  $26/365 \times \$3620 = \$260/\text{yr}$ .
- S Electricity use by each probe is 25 VA.  $25 \times 1.732 \times 0.9 \text{ PF} \times 0.001 = 0.039 \text{ kW}$  0.039 for 16 probes is 0.62 kW.  $0.62 \text{ kW} \times 24 \text{ hr/d} \times \$0.05/\text{kWH} = 0.74/\text{d}$  $0.74/\text{d} \times 365 = \$272/\text{Jyr}$
- Total cost of 16 probes

concentrations with the target MLSS, and made manual valve adjustments through the computer.

After staff felt comfortable that the MLSS probe device was collecting accurate data, they discontinued daily grab sampling and lab analyses altogether. The computer loop was modified to actuate the WAS flow valve, eliminating the need for manual adjustment. Related to a setpoint MLSS, the probe device signals the valve to adjust its opening, allowing for automated, constant MLSS control.

Automatic wasting can be achieved in a DCS system either by a sophisticated proportional integral derivative loop control system or by an algorithm. The following equation is a modification of the previous wasting rate equation and uses the 24-hour average actual MLSS as determined by the probe device.

New  $Q_{WAS}$  = Previous  $Q_{WAS}$ × [actual MLSS (24-hr average)/target MLSS]<sup>0.5</sup>

trolled basins, the on-line basin was suworked well when using MLSS conmal scum and good color. In March was improved aesthetically with minibasin with constant MLSS control also perior in maintaining MLSS concentra-Compared with the manually concentrations measured by the probeusing wasting instructions calculated plemented in all seven active basins 1997, constant MLSS control was imtions near target levels. the two test basins. from the data acquired from probes in The operators found the algorithm The on-line

### **Better and Cost Effective**

A comparison of ammonia removal from rotal plant flow before and after constant MLSS control shows that am-



MLSS probes. The probes provide a more accurate measurement of suspended solids Return activated sludge (RAS) probes and transmitter box were installed along with in RAS than grab samples.

monia levels have been consistent and well below National Pollutant Discharge Elimination System permit limits. Phosphorus removal also improved in consistency and reliability, as demonstrated by the two basins that had been working off of the probes since early 1996.

A cost evaluation was prepared to determine the benefit of implementa-

tion of a fully automated control system with probes in all basins (see table, p. 24). Annualized capital costs were estimated to be \$91 000/yr, and annual cost savings were approximately \$29 000/yr with a payback period of 3 years. The district felt that the improved nutrient removal, coupled with the cost savings of reduced operator attention and lab time, was

enough to warrant the switch to fully automated control. As a result of making the switch, the plant also has reduced ferric chloride use. When considering savings due to reduced ferric addition and resulting solids production and disposal, the payback period is 0.5 to 1.3 years.

## A Step Beyond MLSS Control

Every operator dreams of achieving a constant solids retention time (SRT), particularly for situations in which extreme flow variations flush solids through the aeration basin. SRT is calculated as pounds of solids under aeration (based on MLSS), divided by pounds of solids wasted per day (based on RASSS). The use of

method as the preferred process control and is using automated constant SRT stalled RASSS probes in all basins MLSS. constant SRT provides better control SRT control. tions provides for automatic constant ing of RASSS and MLSS concentra-MLSS does not. Automatic monitorconcentration, whereas constant and is adjustable to changes in WAS cause SRT is a better parameter than over the activated sludge process be-Constant SRT accounts for The district has in-

The use of on-line suspended solids probes can greatly enhance process control in activated sludge systems and can specifically improve the reliability and stability of BNR

processes. In addition, Clark County found that the costs of probe installation, operation, and maintenance are far less than manual sample collection, lab analyses, and subsequent calculations and manual equipment adjustments. The automated method can be readily implemented at facilities with SCADA systems or those suited to a computer-controlled wasting process.

Robin E. Bain, now with Parsons Engineering Science in Las Vegas, Nev., was plant operations manager from 1993 to 1996, and Walter S. Johnson is a process control specialist at Clark County Sanitation District in Las Vegas.

